

## Solid-liquid separation

Solid-liquid separation processes play an important role in the processing of bio-based products. For example, digestate has to be separated from fermentation broths, and sludges as well as microalgae need to be dewatered. For that purpose, continuous, mechanical processes like decanter centrifugation and filtration are the established methods in industrial applications. At DBFZ, the following equipment for solid-liquid separation is available in pilot scale:



Decanter centrifuge



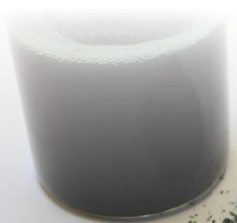
Hydraulic filter press

### Decanter centrifuge:

- Centrifugal acceleration up to 4.400 g
- Capacity up to 100 L h<sup>-1</sup>
- Complete mass and energy balances

### Hydraulic filter press:

- Compacting pressure up to 60 bar
- Pressure chamber approx. 2 L



## Liquid-liquid separation

Biorefinery products, such as fuels or fine and platform chemicals, are often present as liquids. The DBFZ uses liquid-liquid separation processes to separate and concentrate these products from their aqueous environments as well as fractionate them from each other. For practical investigations, pilot plants for membrane filtration, liquid-liquid extraction, and adsorption are available. High-quality products or very similar components can furthermore be purified with a preparative high-performance liquid chromatography (HPLC).



Membrane filtration



Liquid-liquid extraction

### Membrane filtration:

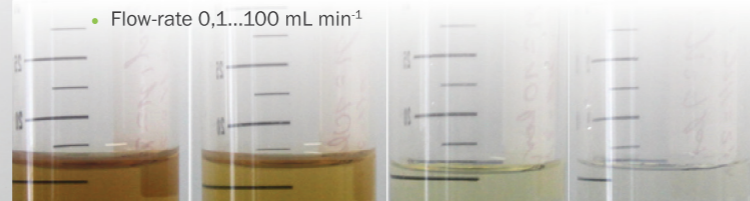
- Micro-, ultra-, nanofiltration and reverse osmosis
- Polymer and ceramic membranes
- $p_{max} = 60 \text{ bar}$ ,  $T = 20...90 \text{ °C}$ ,  $CF = 5...31 \text{ L min}^{-1}$

### Liquid-liquid extraction:

- Stirred and heated countercurrent extraction
- $h = 1600 \text{ mm}$ ,  $d = 25 \text{ mm}$ ,  $V_{Feed} = 15 \text{ L}$

### Preparative HPLC:

- Separation of sugars, furan derivatives, phenols and organic acids etc.
- Flow-rate 0,1...100 mL min<sup>-1</sup>



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## Further information

Further information can be found at [www.dbfz.de](http://www.dbfz.de)

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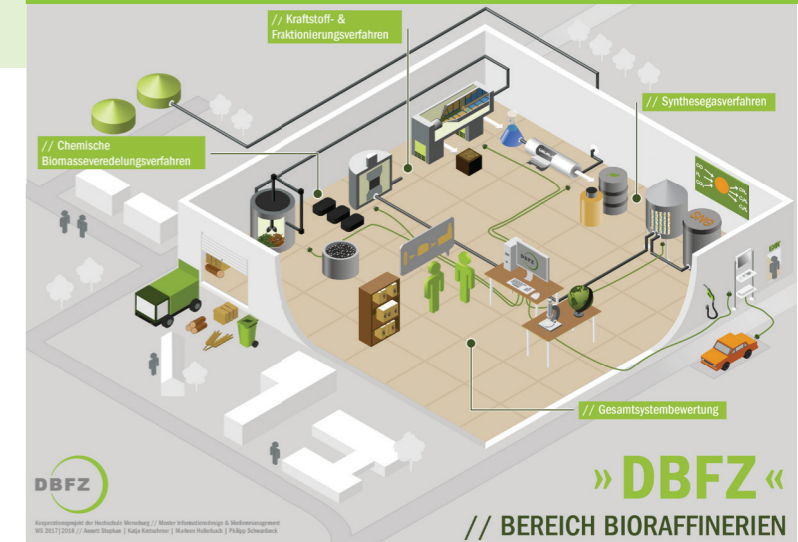
SAB Sächsische AufbauBank



Europa fördert Sachsen. EFRE Europäischer Fonds für regionale Entwicklung



## Biorefinery Laboratory



Hydrothermal processes, Gasification, Gas cleaning, Synthesis, Separation processes

## Hydrothermal processes



Hydrothermal processes (HTP) are generally defined as thermochemical transformations in hot compressed water (180 – 350 °C / 20 – 200 bar). Water is important for such processes, since it acts as solvent and reaction medium at the same time. Biomasses, such as sewage sludge, digestate, as well as hydrolysates from lignocellulosic

residues, contain large amounts of water. Therefore, HTP are a promising technology in biorefinery concepts for the conversion of wet feedstock's to high-value solid, liquid and gaseous products. For hydrothermal investigations, the following laboratory plants are available:

### Discontinuous stirred tank reactors (DSTR):

- 500 mL / electrically heated  
 $T_{\max} = 300 \text{ °C}$ ,  $p_{\max} = 200 \text{ bar}$ ,  $Q_{\text{el}} = 3 \text{ kW}$
- 500 mL thermostatically heated  
 $T_{\max} = 270 \text{ °C}$ ,  $p_{\max} = 200 \text{ bar}$ ,  $Q_{\text{th}} = 3,5 \text{ kW}$
- 10 L thermostatically heated  
 $T_{\max} = 300 \text{ °C}$ ,  $p_{\max} = 150 \text{ bar}$ ,  $Q_{\text{th}} = 7 \text{ kW}$

### Continuous laboratory plants:

- Tube reactor ( $l = 860 \text{ mm}$ ,  $d_i = 20 \text{ mm}$ )  
 $T_{\max} = 350 \text{ °C}$ ,  $p_{\max} = 200 \text{ bar}$
- 2-stage hydrothermal laboratory plant  
1<sup>st</sup> stage:  $T_{\max} = 350 \text{ °C}$ ,  $p_{\max} = 200 \text{ bar}$   
→ hydrothermal biomass decomposition  
2<sup>nd</sup> stage:  $T_{\max} = 300 \text{ °C}$ ,  $p_{\max} = 100 \text{ bar}$   
→ refining

## Biomass gasification

Solid and dry biomass can be converted to synthesis gas by means of biomass gasification. This thermo-chemical process needs high temperatures as well as sub-stoichiometric addition of gasification agents, e.g. air or steam, and is characterized by maximum carbon conversion. The recovered synthesis gas, which consists of the main components carbon monoxide, hydrogen, carbon dioxide and methane, can be used for combined heat and power generation and for the production of various chemical energy carriers/fuels and basic chemicals after cleaning. Various reactors with extensive measurement technology are available for the gasification of biomass.



### Entrained flow gasifier:

- $T_{\max} = 1200 \text{ °C}$ ,  $p = 1 \text{ bar}$
- Up to  $3 \text{ kg h}^{-1}$  fuel

### Fixed bed gasifier:

- $T_{\max} = 950 \text{ °C}$ ,  $p_{\max} = 20 \text{ bar}$
- Gasification agent: Air,  $\text{N}_2/\text{O}_2$ , steam,  $\text{CO}_2$

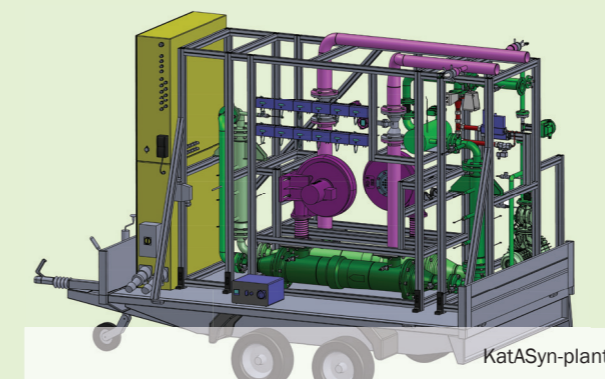
### Gas analytics:

- Gas chromatography (GC-TCD, GC-FID), FTIR spectrometry



## Gas cleaning

To be able to use product gases of the biomass gasification for the provision of power and heat (cogeneration of heat and electricity) or fuels / chemicals (synthesis), a gas cleaning necessary. Pollutants to be separated, are here solid particle (dust), hydrocarbons (tar), sulfur and halogenide /nitrogen-components ( $\text{H}_2\text{S}$ ,  $\text{HCl}$ ,  $\text{HCN}$ ) and alkalis. According to application different gas quality different limit values must to be observed. For gas cleaning the following test states are available:



### KatASyn-plant:

- $T_{\max} = 900 \text{ °C}$ ,  $p = 1 \text{ bar}$
- Gasflow up to  $15 \text{ m}^3 \text{ h}^{-1}$  (STP) (correspond to 20 kW fuel power)
- 2-stage: reforming and adsorption
- Mobile installation in car trailer

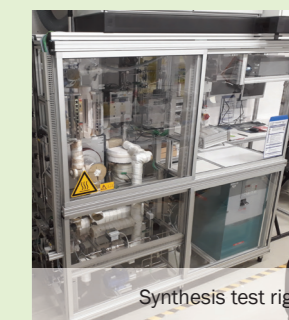
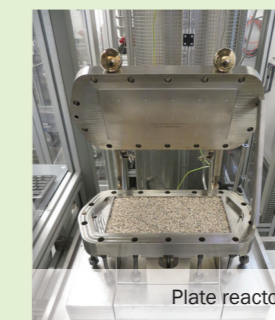
### Adsorptiv cleaning plant:

- $T_{\max} = 350 \text{ °C}$ ,  $p = 1 \text{ bar}$
- Gasflow Up to  $5 \text{ m}^3/\text{h}$  (STP)
- 3 fixed bed for hydrogenation catalyst, impregnated activated carbon plus Zinc- and Copper-sorbents.



## Syngas technologies

Cleaned and conditioned synthesis gas is converted catalytically into synthetic natural gas (SNG), light alkene (ethane, propene) or synthetic fuels in our lab. The test rigs displayed below allow to compare different reactor concepts as well as commercial and newly developed catalysts at industrially relevant conditions. Two test rigs with two reactors each are applied to develop new synthesis processes, study the kinetics of catalysts and analyse the non-stationary operation of synthesis reactors. New catalysts are developed in cooperation with an industrial catalyst manufacturer.



### Three tube reactors with recycle cooling:

- Electrically heated:  $T_{\max} = 850 \text{ °C}$ ,  $p_{\max} = 60 \text{ bar}$
- Electrically heated:  $T_{\max} = 550 \text{ °C}$ ,  $p_{\max} = 10 \text{ bar}$
- Oil tempered:  $T_{\max} = 350 \text{ °C}$ ,  $p_{\max} = 1,5 \text{ bar}$

### Plate reactor:

- $T_{\max} = 350 \text{ °C}$ ,  $p_{\max} = 20 \text{ bar}$
- Heating and cooling with thermal oil

### Gas analytics:

- Gas chromatography (GC-TCD, GC-FID), FTIR spectrometry

